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# **PATENT**

# IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In Re Reissue Application of:

Atty. Docket

No.:

9323.00001

U.S. Patent No. 5,788,864

8,864

Issued:

August 4, 1998

Application No.:

09/632,812

Group Art Unit:

1761

Filed:

August 4, 2000

Examiner:

Chester T. Berry

For:

AMINE HEAT STABLE SALT REMOVAL FROM TYPE II ANION EXCHANGE RESIN

#### **STATUS INQUIRY**

#### CUSTOMER WINDOW, MAIL STOP REISSUE

U.S. Patent and Trademark Office 220 20<sup>th</sup> Street S. Crystal Plaza Two, Lobby, Room 1B03 Arlington, VA 22202

Sir:

Applicants request an update on the status of the above-identified application. A Response to Non-Compliant Amendment submitting a revised Listing of Claims was filed on August 6, 2004. For the Examiner's convenience, a courtesy copy of the response filed and the stamp receipt postcard is attached.

Please advise us of the status of the above-identified application, including an indication as to when the next communication can be expected. We look forward to your reply.

Respectfully submitted,

Date: November 3, 2

By:

William J. Fisher

Registration No. 32,133

Banner & Witcoff, Ltd. 1001 G Street, N.W.

Washington, D.C. 20001-4597

(202) 824-3000

Attachment: Response filed August 6, 2004

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# RESPONSE TO NON-COMPLIANT AMENDMENT

#### CUSTOMER WINDOW, MAIL STOP REISSUE

U.S. Patent and Trademark Office 220 20<sup>th</sup> Street S. Crystal Plaza Two, Lobby, Room 1B03 Arlington, VA 22202

Sir:

In response to the Notice of Non-Compliant Amendment mailed March 9, 2004, Applicant submits herewith a replacement "Listing of Claims" portion of the Amendment filed on September 10, 2003. It is believed that the submission of the revised Listing of Claims is in full compliance with the rules under 37 C.F.R. §§ 1.121(b) (ii) and 1.121(b)(iii). Applicants petition for a four (4) month extension of the term and authorizes the charging of the \$1,480 fee to our Deposit Account No. 19-0733.

Respectfully submitted,

COPY

Date:

tugust 6,2004

By:

William J. Fisher

Registration No. 32,133

Banner & Witcoff, Ltd. 1001 G Street, N.W. Washington, D.C. 20001-4597

(202) 824-3000

Attachment: Listing of Claims

Application No. 09/632,812 Amendment dated September 10, 2003 Reply to Office Action of March 20, 2003 Client/Matter No. 09323,00001

**Listing of Claims:** 

Claim 1 (previously presented) A process for regenerating a Type II strong base anion

exchange resin comprising:

passing an alkanolamine solution, whose effectiveness at removing H<sub>2</sub>S and CO<sub>2</sub> from

gas streams has been decreased by the accumulation of heat stable salts, through a bed of Type II

strong base anion exchange resin until the active anion exchange sites of said Type II strong base

anion exchange resin are loaded with heat stable salt anions; and

contacting said loaded Type II resin with an amount of an alkali metal hydroxide and for

a time sufficient to obtain recovery of over 50% of the virgin capacity of the loaded Type II

resin.

Claim 2 (previously presented) The process according to claim 1 wherein said heat stable

salt anion is SCN.

Claim 3 (previously presented) The process according to claim 1 wherein said alkali

metal hydroxide is sodium hydroxide.

Claim 4 (previously presented) The process according to claim 3 wherein the amount of

sodium hydroxide is from about 1 to about 40 pounds of NaOH equivalent per cubic foot of

resin.

Claim 5 (previously presented) A process for regenerating a Type II strong base anion

exchange resin comprising:

passing an alkanolamine solution, whose effectiveness at removing H<sub>2</sub>S and CO<sub>2</sub> from

gas streams has been decreased by the accumulation of heat stable salts, through a bed of Type II

strong base anion exchange resin until the active anion exchange sites of said Type II strong base

anion exchange resin are loaded with heat stable salt anions;

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Client/Matter No. 09323.00001

contacting said loaded Type II resin with an amount of an alkali metal hydroxide and for

a time sufficient to obtain recovery of over 50% of the virgin capacity of the loaded Type II

resin; and

repeating the steps of loading said Type II resin with said anions and regenerating

repeatedly without substantial further reduction in active anion exchange sites.

Claim 6 (previously presented) The process according to claim 5 wherein said heat stable

salt anion is SCN<sup>-</sup>.

Claim 7 (previously presented) The process according to claim 5 wherein said alkali

metal hydroxide is sodium hydroxide.

Claim 8 (previously presented) A process consisting of:

loading a Type II strong base anion exchange resin with SCN;

washing said Type II anion resin with water;

regenerating said Type II anion exchange resin in a single step with a solution of sodium

hydroxide having a concentration of from about 1% to about 15% by weight of sodium

hydroxide at a temperature of from about 70°F. to about 120°F. in an amount of NaOH from

about 5 to about 35 pounds per cubic foot for from about 5 to about 120 minutes to remove heat

stable anions from said resin to obtain recovery of over 50% of the virgin capacity of the loaded

Type II resin; and

washing said Type II anion exchange resin with water.

Claim 9 (currently amended) A cyclic process for purifying an aqueous alkanolamine

solution containing alkali metal salts of anions which form heat stable salts with alkanolamines,

heat stable salts of such anions with alkanolamines, or both, comprising:

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- (a) contacting the aqueous alkanolamine solution with a Type II strong base anion exchange resin to transfer at least some heat stable salt anions from the solution to the resin;
- (b) regenerating the resin by contacting the resin with an alkali metal hydroxide so that the alkali metal hydroxide removes from the resin substantially all-the same quantity of heat stable salt anions transferred to the resin in step (a); and
- (c) repeating steps (a) and (b).

Claim 10 (previously presented) The process according to claim 9 wherein said alkali metal hydroxide is sodium hydroxide.

Claim 11 (previously presented) The process according to claim 9 wherein said aqueous alkanolamine solution is approximately 40% by weight alkanolamine.

Claim 12 (currently amended) A process for purifying an aqueous alkanolamine solution containing alkali metal salts of anions which form heat stable salts with alkanolamines, heat stable salts of such anions with alkanolamines, or both obtained from contacting the aqueous alkanolamine solution with a hydrocarbon gas stream containing acid gasses, comprising:

- (a) contacting the aqueous alkanolamine solution with a Type II strong base anion exchange resin to transfer at least some heat stable salt anions from the solution to the resin;
- (b) recirculating the aqueous alkanolamine solution recovered from step (a) to contact the hydrocarbon gas stream containing acid gasses;
- (c) regenerating the resin by contacting the resin with an alkali metal hydroxide so that the alkali metal hydroxide removes from the resin substantially all-the same quantity of heat stable salt anions transferred to the resin in step (a); and
- (d) repeating steps (a) (c).

Application No. 09/632,812 Amendment dated September 10, 2003 Reply to Office Action of March 20, 2003 Client/Matter No. 09323.00001

Claim 13 (New) The method of claim 9, wherein the heat stable salts comprise thiocyanate.

Claim 14 (New) The method of claim 12, wherein the heat stable salts comprise thiocyanate.



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